

VISCOMETRIC STUDY ON BINARY LIQUID MIXTURES OF PROPIOPHENONE WITH ANILINE AND N-ALKYL SUBSTITUTED ANILINES, AT 303.15 TO 318.15 K

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ABSTRACT

Densities and viscosities of binary mixtures of Propiophenone with Aniline, N-methylaniline, N, N- dimethylaniline, N, N- diethylaniline were measured over the entire composition range at $T = (303.15 \text{ to } 318.15) \text{ K}$ (with 5K interval) and atmospheric pressure. Experimental data were used to calculate the deviation of viscosity $\Delta\eta$, excess Gibb's free energy G^*E activation of viscous flow for each binary system, and these excess thermodynamic properties were fitted to the Redlich-Kister polynomial equation to obtain the fitting coefficients and standard deviations. McAllister's three-body /four-body interaction models were used for the correlation of viscosity data. The studied systems exhibit good intermolecular interactions due to hydrogen ion transfer and charge dispersion in the carbonyl group and NH₂ groups of Aniline and Alkyl Substituted Anilines. Experimental results are useful in various pharmaceutical industries.

Keywords: Viscosity, Deviation in Viscosity, McAllister's Models, Viscosity Relations.

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INTRODUCTION

Viscosity properties of the binary liquid mixtures are important for fluid transport, chemical industries, pharmaceutical processes, and food products. Excess thermodynamic properties of the binary liquid mixtures of Propiophenone with Aniline, N-Methylaniline, N, N- Dimethyl aniline and N, N-Diethyl aniline were calculated based on the values of densities, ρ , and viscosities, η , over the entire composition range at $T = (303.15 \text{ to } 318.15) \text{ K}$. Propiophenone is used as an intermediate in the industrial processes.¹ Aromatic anilines and substituted alkyl anilines are also useful in making dyes. Literature survey reveals some studies on Aniline with other compounds.²⁻⁷ Hence, no studies were made on the current binary mixtures. Measured values of density and viscosity data were used to calculate $\Delta\eta$, one interaction parameters of d_{12} , G^*E , W_{vis}/RT , H_{12} , and T_{12} , (Grunberg and Nissan, Gibb's free energy, Katti and Chaudhary, Hind et.al., and Tamara-Kurata respectively) for the studied binary liquid mixtures. McAllister's three and four body, Auslander and Jouyban-Acree relations for two and three adjustable interaction parameter equations were used to correlate and to understand the intermolecular interactions. Experimental viscosity data was compared with the calculated values of having no adjustable parameter relations such as Bingham, Arrhenius, Kendall and Monroe, and Kendall. The values of $\Delta\eta$ and G^*E of binary mixtures were fitted to the Redlich Kister polynomial equation to estimate the coefficients and standard deviations between the experimental and theoretical values.

EXPERIMENTAL

The purities of the selected solvents are as shown in Table-1 and they are purchased from S.D. Fine chemicals Ltd, India.

Table -1: Provenance and Purity of the Materials Used

Chemicals	CAS number	Source	Mass Fraction Purity
Propiophenone (PPH)	93-55-0	S.D fine Chemicals, India	99.0%
Aniline (A)	62-53-3	S.D fine Chemicals, India	99.7%
N-Methylaniline (MA)	100-61-8	S.D fine Chemicals, India	99.5%
N,N-Diethylaniline (DMA)	91-66-7	S.D fine Chemicals, India	99.6%
N,N-Dimethylaniline (DEA)	121-69-7	S.D fine Chemicals, India	99.5%

The water content was less than 0.003 mass%. Mettler Toledo (ME204) balance was used to weigh the pure liquids and prepare the liquid mixtures, precision of ± 0.1 mg. The experimental and literature values of densities and viscosities of the liquids are given in Table-2, a⁸, b⁹, c¹⁰, d¹¹, e¹¹, f⁷, g¹², h⁷, i¹, j¹³, k¹⁴, l², m¹⁵, n¹⁶, o¹⁷, p¹⁸, q¹⁹, r²⁰.

Table -2: Comparison of Experimental Density and Viscosity of Pure Liquid with Literature Values

Compound	T(K)	Density (ρ)		ref	Viscosity(η)		ref
		Experimental	Literature		Experimental	Literature	
		gm/cm ³	gm/cm ³		mpa.s	mpa.s	
Propiophenone	303.15	1.0045	1.0044	j	1.5150	1.5100	h
	308.15	1.0015	1.0060	j	1.4690	1.4690	i
	313.15	0.9985			1.4230		
	318.15	0.9955			1.3770		
Aniline	303.15	1.0128	1.0130	a	3.191	3.746	n
			1.0128	b		3.770	n
			1.0128	e		3.190	l
			1.0129	l		3.190	q
			1.0132	r			
	308.15	1.0089	1.0087	l	2.811	2.800	l
N-Methylaniline	313.15	1.0049	1.0049	e	2.436	2.420	l
			1.0049	k			
	318.15	1.0009			2.065		
	303.15	0.9783	0.9817	c	1.963	1.965	c
			0.9782	e		1.963	d
N,N-Diethylaniline			0.9783	m			
	308.15	0.9740	0.9742	p	1.811		
	313.15	0.9696	0.9696	e	1.658		
	318.15	0.9652			1.504		
	303.15	0.9479	0.9480	l	1.173	1.174	l
	308.15	0.9436	0.9517	f	1.078	1.090	l
			0.9518	g		1.111	l
N,N-Dimethylaniline			0.9436	l			
	313.15	0.9393	0.9394	l	0.981	0.982	l
	318.15	0.9351			0.885		
	303.15	0.9260	0.9260	p	1.703	1.703	p
			0.9253	a		1.711	a
			0.9260	o		1.703	o
	308.15	0.9217	0.9213	a	1.554	1.548	a
			0.9219	o		1.550	o
N,N-Dimethylaniline	313.15	0.9176	0.9177	p	1.406	1.402	p
			0.9175	o			
	318.15	0.9134			1.263		

Apparatus and Procedures

Anton Paar (DSA 5000 M) oscillating u-tube densimeter, automatically thermostatic within $\pm 0.01\text{K}$, was used to measure the densities of the pure components and the binary mixtures over the whole composition range $T = (303.15 \text{ to } 318.15) \text{ K}$. Averages of five measurements were taken at temperatures from 303.15 to 318.15K with an increment of 5K under atmospheric pressure. The standard uncertainties were found to be $\pm 0.001 \text{ kg.m}^{-3}$ and $\pm 0.005 \text{ mPa.s}$ for the measurements of density and viscosity respectively. The Ubbelohde viscometer was used to measure the Viscosity as per the method described earlier.²¹ The measured values of densities²², viscosities, and calculated values of deviation in viscosity and Gibbs free energy values with respective mole fractions of the studied binary mixtures at $T = 303.15 \text{ to } 318.15\text{K}$ are tabulated in Table-3 and Table-4.

RESULTS AND DISCUSSION

Negative values of deviation in viscosity ($\Delta\eta$) were observed and they were decreasing with the increase in temperature for all the studied binary mixtures. The difference in size and shape of the component molecules and the loss of dipolar association in pure components was the reason and it is in line with Fort and Moore (1966) and Pikkarainen (1983). The deviation in viscosity values are maximum at the mole fractions 0.5069, 0.4826, 0.4880 and 0.5447 are -0.0309, -0.0340, -0.0368 and -0.0416 for PPH+Aniline, PPH+MA, PPH+DMA and PPH+DEA at 303.15K, 313.15K and it is shown in the Figures-1-2. The order of interactions for deviation in viscosity is $\text{PPH+A} > \text{PPH+MA} > \text{PPH+DMA} > \text{PPH+DEA}$.

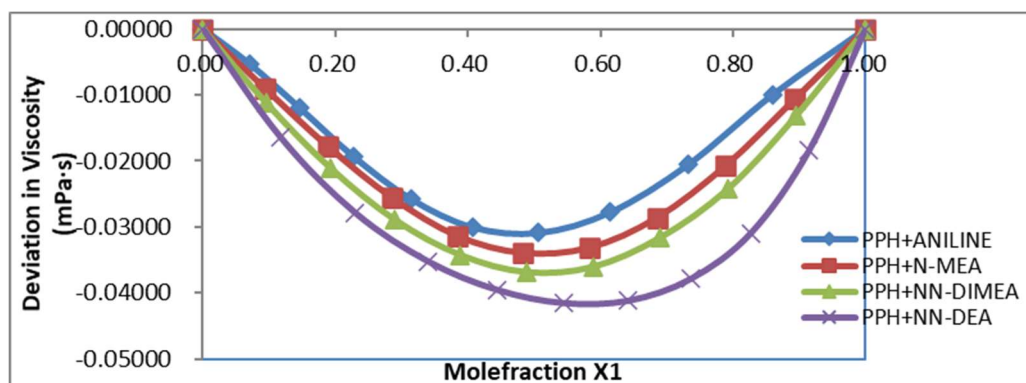


Fig.-1: Deviation in Viscosity Values of the Binary Mixtures Propiophenone with Aniline, N-Methylaniline, N, N-Dimethylaniline, N, N-Diethylaniline concerning their Mole Fraction Values at $T = 303.15 \text{ K}$.

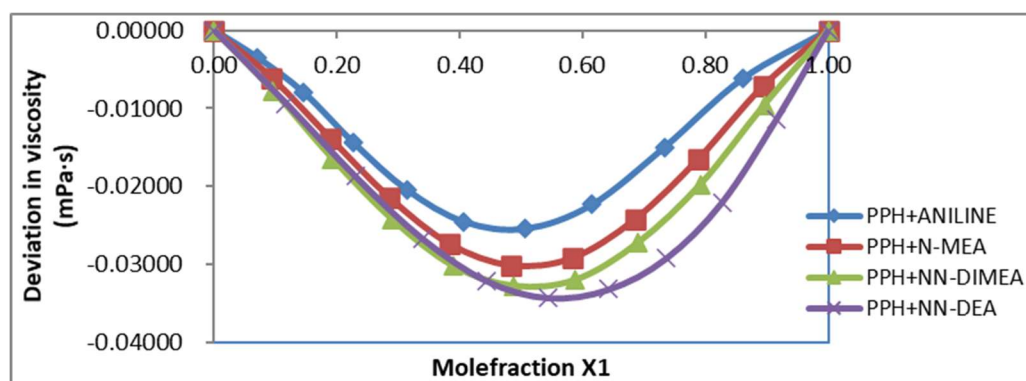


Fig.-2: Deviation in Viscosity Values of the Binary Mixtures Propiophenone with Aniline, N-Methylaniline, N, N-Dimethylaniline, N, N-Diethylaniline concerning their Mole Fraction Values at $T = 313.15 \text{ K}$.

The presence of weak interactions between unlike molecules indicates a negative value of d_{12} and the presence of specific interactions indicates positive d_{12} values as per Moore et al²³ and Ramamoorthy.²⁴ Positive values of both deviations in viscosity, $\Delta\eta$, and Grunberg-Nissan parameter d_{12} indicates the

presence of strong specific interactions, negative $\Delta\eta$ and positive d_{12} indicates weak specific interactions, negative values of both $\Delta\eta$ and d_{12} indicates the absence of specific interactions as per Nigam and Mahal.²⁵

Table -3 Density, Viscosity, Deviation in Viscosity and Gibbs Free Energy Values for the Binary Mixtures of Propiophenone with Aniline, N-Methylaniline, N, N-Dimethyl aniline & N, N-Diethyl aniline with respective Mole Fractions at T=(303.15- 308.15)K.

X1	303.15K				308.15K			
	ρ	η	$\Delta\eta$	G*E	ρ	η	$\Delta\eta$	G*E
	gm/cm ³	mPa·s	mPa·s	J/mol	gm/cm ³	mPa·s	mPa·s	J/mol
PPH+ANILINE								
0.0000	1.0128	3.1911	0.0000	0.0000	1.0089	2.8107	0.0000	0.0000
0.0708	1.0122	3.0067	-0.0053	0.4474	1.0083	2.6447	-0.0041	0.3695
0.1463	1.0115	2.8279	-0.0120	0.8470	1.0078	2.4844	-0.0095	0.6934
0.2270	1.0109	2.6517	-0.0193	1.1885	1.0072	2.3286	-0.0158	0.9623
0.3136	1.0101	2.4794	-0.0257	1.4669	1.0065	2.1832	-0.0212	1.1772
0.4066	1.0093	2.3112	-0.0300	1.6688	1.0059	2.0447	-0.0252	1.3237
0.5069	1.0085	2.1458	-0.0309	1.7765	1.0051	1.9131	-0.0259	1.3969
0.6152	1.0076	1.9831	-0.0277	1.7533	1.0043	1.7889	-0.0232	1.3682
0.7327	1.0066	1.8259	-0.0205	1.5388	1.0034	1.6743	-0.0164	1.2009
0.8605	1.0056	1.6709	-0.0099	1.0284	1.0025	1.5684	-0.0072	0.8049
1.0000	1.0045	1.5150	0.0000	0.0000	1.0015	1.4690	0.0000	0.0000
PPH+N-METHYL ANILINE								
0.0000	0.9783	1.9630	0.0000	0.0000	0.9740	1.8105	0.0000	0.0000
0.0939	0.9816	1.9036	-0.0091	-0.0157	0.9775	1.7530	-0.0072	-0.0251
0.1891	0.9848	1.8467	-0.0179	-0.0552	0.9809	1.7035	-0.0160	-0.0923
0.2856	0.9878	1.7930	-0.0256	-0.1061	0.9840	1.6604	-0.0236	-0.1619
0.3834	0.9907	1.7429	-0.0314	-0.1559	0.9870	1.6213	-0.0294	-0.2257
0.4826	0.9933	1.6967	-0.0340	-0.1857	0.9898	1.5864	-0.0320	-0.2616
0.5831	0.9958	1.6551	-0.0332	-0.1916	0.9924	1.5550	-0.0312	-0.2643
0.6852	0.9981	1.6175	-0.0286	-0.1646	0.9949	1.5274	-0.0265	-0.2216
0.7886	1.0003	1.5833	-0.0207	-0.1104	0.9972	1.5031	-0.0186	-0.1448
0.8935	1.0024	1.5501	-0.0106	-0.0455	0.9994	1.4844	-0.0089	-0.0572
1.0000	1.0045	1.5150	0.0000	0.0000	1.0015	1.4690	0.0000	0.0000
PPH+N, N-DIMETHYLANILINE								
0.0000	0.9479	1.1730	0.0000	0.0000	0.9436	1.0778	0.0000	0.0000
0.0958	0.9538	1.1985	-0.0112	-0.1640	0.9498	1.1068	-0.0089	-0.0966
0.1925	0.9599	1.2243	-0.0211	-0.3095	0.9560	1.1370	-0.0183	-0.2203
0.2900	0.9659	1.2511	-0.0289	-0.4217	0.9621	1.1688	-0.0261	-0.3217
0.3886	0.9717	1.2802	-0.0342	-0.4912	0.9681	1.2030	-0.0317	-0.3918
0.4880	0.9774	1.3124	-0.0368	-0.5176	0.9739	1.2402	-0.0343	-0.4159
0.5885	0.9830	1.3475	-0.0360	-0.4920	0.9796	1.2803	-0.0335	-0.3917
0.6899	0.9884	1.3863	-0.0316	-0.4146	0.9851	1.3233	-0.0291	-0.3210
0.7922	0.9937	1.4278	-0.0242	-0.3042	0.9906	1.3692	-0.0214	-0.2164
0.8956	0.9990	1.4713	-0.0131	-0.1529	0.9960	1.4180	-0.0109	-0.0951
1.0000	1.0045	1.5150	0.0000	0.0000	1.0015	1.4690	0.0000	0.0000
PPH+N,N-DIETHYLANILINE								
0.0000	0.9260	1.7030	0.0000	0.0000	0.9217	1.5544	0.0000	0.0000
0.1173	0.9340	1.6645	-0.0165	-0.1907	0.9300	1.5315	-0.0129	-0.1685
0.2302	0.9421	1.6318	-0.0279	-0.3321	0.9382	1.5114	-0.0234	-0.3152
0.3389	0.9502	1.6041	-0.0352	-0.4284	0.9464	1.4946	-0.0308	-0.4257
0.4437	0.9582	1.5800	-0.0396	-0.4932	0.9545	1.4807	-0.0358	-0.5040
0.5447	0.9661	1.5590	-0.0416	-0.5317	0.9626	1.4699	-0.0380	-0.5435
0.6422	0.9739	1.5411	-0.0412	-0.5406	0.9705	1.4624	-0.0372	-0.5402
0.7363	0.9816	1.5267	-0.0379	-0.5092	0.9783	1.4580	-0.0335	-0.4927
0.8272	0.9892	1.5166	-0.0309	-0.4252	0.9861	1.4574	-0.0264	-0.3904
0.9150	0.9968	1.5126	-0.0183	-0.2560	0.9938	1.4614	-0.0148	-0.2203

X1	303.15K				308.15K			
	ρ	η	$\Delta\eta$	G*E	ρ	η	$\Delta\eta$	G*E
	gm/cm ³	mPa·s	mPa·s	J/mol	gm/cm ³	mPa·s	mPa·s	J/mol
1.0000	1.0045	1.5150	0.0000	0.0000	1.0015	1.4690	0.0000	0.0000

Table -4 Density, Viscosity, Deviation in Viscosity and Gibbs Free Energy Values for the Binary Mixtures of Propiophenone with Aniline, N-Methylaniline, N, N-Dimethyl aniline & N, N-Diethyl aniline with respective Mole Fractions at T=(313.15- 318.15)K.

X1	313.15K				318.15K			
	ρ	η	$\Delta\eta$	G*E	ρ	η	$\Delta\eta$	G*E
	gm/cm ³	mPa·s	mPa·s	J/mol	gm/cm ³	mPa·s	mPa·s	J/mol
PPH+ANILINE								
0.0000	1.0049	2.4360	0.0000	0.0000	1.0009	2.0650	0.0000	0.0000
0.0708	1.0044	2.2874	-0.0035	0.2848	1.0005	1.9323	-0.0027	0.2034
0.1463	1.0040	2.1460	-0.0080	0.5292	1.0001	1.8071	-0.0072	0.3592
0.2270	1.0035	2.0118	-0.0144	0.7120	0.9997	1.6958	-0.0136	0.4566
0.3136	1.0029	1.8920	-0.0204	0.8449	0.9992	1.6011	-0.0196	0.5155
0.4066	1.0023	1.7806	-0.0245	0.9306	0.9987	1.5208	-0.0237	0.5455
0.5069	1.0016	1.6833	-0.0254	0.9676	0.9982	1.4540	-0.0246	0.5539
0.6152	1.0009	1.5968	-0.0223	0.9456	0.9976	1.4060	-0.0215	0.5414
0.7327	1.0002	1.5251	-0.0150	0.8404	0.9970	1.3756	-0.0142	0.4968
0.8605	0.9994	1.4689	-0.0062	0.5711	0.9963	1.3690	-0.0054	0.3565
1.0000	0.9985	1.4230	0.0000	0.0000	0.9955	1.3770	0.0000	0.0000
PPH+N-METHYL ANILINE								
0.0000	0.9696	1.6577	0.0000	0.0000	0.9652	1.5040	0.0000	0.0000
0.0939	0.9733	1.6049	-0.0061	-0.0386	0.9691	1.4573	-0.0047	-0.0429
0.1891	0.9768	1.5639	-0.0138	-0.1165	0.9727	1.4254	-0.0123	-0.1413
0.2856	0.9801	1.5304	-0.0215	-0.2070	0.9762	1.4026	-0.0197	-0.2471
0.3834	0.9832	1.5027	-0.0274	-0.2869	0.9794	1.3862	-0.0259	-0.3431
0.4826	0.9862	1.4788	-0.0301	-0.3300	0.9825	1.3727	-0.0286	-0.3894
0.5831	0.9889	1.4575	-0.0292	-0.3264	0.9855	1.3629	-0.0276	-0.3796
0.6852	0.9915	1.4401	-0.0242	-0.2671	0.9882	1.3557	-0.0226	-0.3073
0.7886	0.9940	1.4272	-0.0165	-0.1715	0.9908	1.3526	-0.0149	-0.1942
0.8935	0.9963	1.4210	-0.0072	-0.0614	0.9933	1.3591	-0.0060	-0.0670
1.0000	0.9985	1.4230	0.0000	0.0000	0.9955	1.3770	0.0000	0.0000
PPH+N, N-DIMETHYLANILINE								
0.0000	0.9393	0.9807	0.0000	0.0000	0.9351	0.8850	0.0000	0.0000
0.0958	0.9459	1.0134	-0.0077	-0.0388	0.9419	0.9209	-0.0062	0.0509
0.1925	0.9522	1.0481	-0.0165	-0.1248	0.9485	0.9600	-0.0146	0.0074
0.2900	0.9584	1.0849	-0.0243	-0.2106	0.9548	1.0019	-0.0223	-0.0569
0.3886	0.9645	1.1243	-0.0302	-0.2787	0.9609	1.0463	-0.0284	-0.1152
0.4880	0.9704	1.1666	-0.0328	-0.2990	0.9670	1.0937	-0.0312	-0.1363
0.5885	0.9763	1.2117	-0.0320	-0.2784	0.9730	1.1438	-0.0303	-0.1218
0.6899	0.9820	1.2598	-0.0273	-0.2120	0.9788	1.1968	-0.0257	-0.0736
0.7922	0.9876	1.3107	-0.0197	-0.1300	0.9846	1.2525	-0.0179	-0.0143
0.8956	0.9931	1.3654	-0.0096	-0.0392	0.9902	1.3124	-0.0083	0.0296
1.0000	0.9985	1.4230	0.0000	0.0000	0.9955	1.3770	0.0000	0.0000
PPH+N,N-DIETHYLANILINE								
0.0000	0.9176	1.4064	0.0000	0.0000	0.9134	1.2626	0.0000	0.0000
0.1173	0.9260	1.3990	-0.0094	-0.1316	0.9220	1.2686	-0.0074	-0.1010
0.2302	0.9344	1.3915	-0.0187	-0.2745	0.9305	1.2722	-0.0167	-0.2517
0.3389	0.9427	1.3853	-0.0267	-0.4017	0.9389	1.2767	-0.0247	-0.3834
0.4437	0.9509	1.3816	-0.0321	-0.4915	0.9473	1.2832	-0.0301	-0.4748
0.5447	0.9591	1.3812	-0.0343	-0.5294	0.9555	1.2926	-0.0323	-0.5108
0.6422	0.9671	1.3839	-0.0332	-0.5148	0.9637	1.3049	-0.0312	-0.4925
0.7363	0.9751	1.3894	-0.0292	-0.4537	0.9718	1.3196	-0.0272	-0.4277
0.8272	0.9830	1.3981	-0.0220	-0.3415	0.9798	1.3372	-0.0200	-0.3115

X1	313.15K				318.15K			
	ρ	η	$\Delta\eta$	G*E	ρ	η	$\Delta\eta$	G*E
	gm/cm ³	mPa·s	mPa·s	J/mol	gm/cm ³	mPa·s	mPa·s	J/mol
0.9150	0.9908	1.4101	-0.0115	-0.1756	0.9877	1.3578	-0.0095	-0.1413
1.0000	0.9985	1.4230	0.0000	0.0000	0.9955	1.3770	0.0000	0.0000

Computed values of parameters (d_{12} , W_{vis}/RT , H_{12} , T_{12}) are given in Table-5 at temperatures 303.15 K and 313.15 K for the binary mixtures of Propiophenone with Aniline, N-Methylaniline, N, N-Dimethylaniline and N, N-Diethylaniline.

Table-5: Grunberg - Nissan d_{12} , Katti-chaudhari W_{vis}/RT , Hind et.al H_{12} , and Tamara-Kurata T_{12} Constants for the Binary Mixtures of Propiophenone with Aniline, N-Methylaniline, N,N-Dimethylaniline and N,N-Diethylaniline computed by using Viscosity Data over the entire Composition Range at T=303.15K and 313.15K.

X1	d_{12}	W_{vis}/RT	H_{12}	T_{12}	d_{12}	W_{vis}/RT	H_{12}	T_{12}
	303.15K				313.15K			
PPH+ANILINE								
0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
0.0708	0.1993	0.2734	2.3125	2.4964	0.1018	0.1740	1.9029	2.0211
0.1463	0.1998	0.2725	2.3051	2.4684	0.0991	0.1703	1.8975	2.0020
0.2270	0.2010	0.2721	2.2981	2.4403	0.0931	0.1630	1.8885	1.9793
0.3136	0.2041	0.2738	2.2933	2.4141	0.0891	0.1577	1.8821	1.9588
0.4066	0.2098	0.2779	2.2909	2.3902	0.0878	0.1550	1.8787	1.9413
0.5069	0.2191	0.2855	2.2913	2.3696	0.0899	0.1555	1.8787	1.9275
0.6152	0.2328	0.2976	2.2945	2.3522	0.0966	0.1605	1.8824	1.9180
0.7327	0.2525	0.3157	2.3008	2.3385	0.1103	0.1724	1.8912	1.9143
0.8605	0.2827	0.3442	2.3119	2.3305	0.1309	0.1911	1.9037	1.9150
1.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
PPH+N-METHYL ANILINE								
0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
0.0939	-0.0243	-0.0074	1.6858	1.7163	-0.0327	-0.0182	1.5045	1.5232
0.1891	-0.0306	-0.0145	1.6807	1.7066	-0.0449	-0.0305	1.4952	1.5112
0.2856	-0.0366	-0.0209	1.6763	1.6977	-0.0552	-0.0408	1.4877	1.5008
0.3834	-0.0420	-0.0265	1.6726	1.6898	-0.0631	-0.0488	1.4824	1.4926
0.4826	-0.0453	-0.0299	1.6710	1.6842	-0.0673	-0.0531	1.4800	1.4876
0.5831	-0.0470	-0.0317	1.6708	1.6805	-0.0680	-0.0540	1.4803	1.4856
0.6852	-0.0462	-0.0307	1.6727	1.6793	-0.0638	-0.0497	1.4842	1.4876
0.7886	-0.0425	-0.0266	1.6768	1.6808	-0.0555	-0.0413	1.4909	1.4930
0.8935	-0.0354	-0.0192	1.6835	1.6853	-0.0400	-0.0259	1.5027	1.5036
1.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
PPH+N, N-DIMETHYLANILINE								
0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
0.0958	-0.0731	-0.0761	1.2791	1.2770	-0.0111	-0.0180	1.1572	1.1539
0.1925	-0.0759	-0.0800	1.2762	1.2741	-0.0255	-0.0323	1.1489	1.1459
0.2900	-0.0779	-0.0823	1.2737	1.2716	-0.0348	-0.0411	1.1430	1.1401
0.3886	-0.0786	-0.0831	1.2719	1.2699	-0.0409	-0.0471	1.1383	1.1357
0.4880	-0.0788	-0.0832	1.2703	1.2684	-0.0422	-0.0481	1.1362	1.1339
0.5885	-0.0775	-0.0816	1.2696	1.2679	-0.0405	-0.0462	1.1358	1.1337
0.6899	-0.0744	-0.0779	1.2702	1.2688	-0.0343	-0.0398	1.1382	1.1365
0.7922	-0.0717	-0.0742	1.2704	1.2694	-0.0264	-0.0317	1.1419	1.1408
0.8956	-0.0644	-0.0657	1.2740	1.2735	-0.0118	-0.0168	1.1507	1.1501
1.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
PPH+N,N DIETHYLANILINE								
0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
0.1173	-0.0884	-0.0740	1.5295	1.5219	-0.0643	-0.0511	1.3695	1.3722
0.2302	-0.0891	-0.0753	1.5302	1.5243	-0.0753	-0.0622	1.3619	1.3642
0.3389	-0.0902	-0.0768	1.5304	1.5259	-0.0850	-0.0720	1.3552	1.3573
0.4437	-0.0934	-0.0803	1.5288	1.5255	-0.0930	-0.0800	1.3497	1.3517

X1	d ₁₂	W _{vis} /RT	H ₁₂	T ₁₂	d ₁₂	W _{vis} /RT	H ₁₂	T ₁₂
	303.15K				313.15K			
0.5447	-0.0993	-0.0861	1.5252	1.5228	-0.0988	-0.0858	1.3456	1.3476
0.6422	-0.1080	-0.0945	1.5193	1.5179	-0.1031	-0.0900	1.3425	1.3443
0.7363	-0.1193	-0.1054	1.5114	1.5107	-0.1071	-0.0939	1.3395	1.3411
0.8272	-0.1341	-0.1195	1.5009	1.5007	-0.1093	-0.0960	1.3376	1.3388
0.9150	-0.1479	-0.1323	1.4911	1.4912	-0.1042	-0.0907	1.3409	1.3415
1.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000

Table-6: The Standard Deviation Percentages (%) for the Binary Systems at $T=303.15\text{K}$ to 318.15K calculated from the Kendall-Monroe, Bingham, Arrhenius-Eyring's, Kendall Equations.

T/K	Kendall-Munroe	Bingham	Arrhenius	Kendall	Kendall-Munroe	Bingham	Arrhenius	Kendall
	σ (%)	σ (%)	σ (%)	σ (%)	σ (%)	σ (%)	σ (%)	σ (%)
	PPH+ANILINE				PPH+N-MEA			
303.15k	2.22	0.85	8.15	3.74	0.94	1.33	0.17	0.74
308.15K	1.59	0.77	6.65	2.75	1.05	1.31	0.27	0.92
313.15K	0.83	0.82	4.92	1.64	1.14	1.28	0.60	1.07
318.15K	0.17	0.88	3.06	0.56	1.23	1.27	0.94	1.21
	PPH+NN-DMA				PPH+NN-DEA			
303.15k	1.54	1.92	1.57	1.34	1.85	1.93	2.24	1.81
308.15K	1.29	1.85	1.26	1.01	1.79	1.81	2.00	1.78
313.15K	1.04	1.85	0.92	0.64	1.67	1.67	1.67	1.67
318.15K	0.71	1.84	0.47	0.22	1.61	1.66	1.33	1.59

Under the current study, the binary mixture of PPH+Aniline shows positive values of d_{12} and fewer negative values of $\Delta\eta$, it indicates weak specific interactions whereas the other three binary mixtures are having negative values of both $\Delta\eta$ and d_{12} which indicates the absence of specific interactions. Hence, The PPH+Aniline have weak specific interactions, while the other three have no specific interactions, therefore the structural effect is dominant. Under the current study, positive values of G^*E for the binary mixture PPH+Aniline indicate dipole-dipole interactions between the component molecules. The negative values of G^*E for the remaining three binary mixtures show the dispersion forces and it is supported by Reed and Taylor.²⁶ The negative values of the single adjustable parameter of Katti-Chaudhary (W_{vis}/RT) suggest weak interactions and positive values for strong interactions. The values W_{vis}/RT of binary liquid mixture PPH+Aniline are less positive for the entire range of composition, whereas values of W_{vis}/RT for the other three binary liquid mixtures PPH+MA, DMA and DEA are negative.

The single interaction parameter values of Tamara-Kurata, T_{12} , and Hind et.al, H_{12} , don't change considerably from each other. This is in agreement with the Fort and Moore²³. Positive values are observed for all the four binary liquid mixtures over the entire composition range and the values are decreasing with an increase in temperatures from 303.15 to 318.15K. Hence, it shows weak specific interactions.

Average standard deviation percentage ($\sigma\%$) values were calculated and tabulated in Table-5. Amongst all, mixed results were observed. Standard deviation percentage values of Bingham viscosity relation in PPH+A binary mixture, Arrhenius-Eyring's values in PPH+N-MEA binary mixture and Kendall values in PPH+NN-DMA and PPH+NN-DEA binary mixtures are in good agreement with the experimental data, as their $\sigma\%$ values are nearest to zero. McAllister's three/four body equations, Auslander and Jouyban-Acree relations were used to correlate the viscosity data. Two and three adjustable parameters and the standard deviations were calculated with the method of least squares. Interaction coefficients from these relations and standard deviation values are tabulated in Table-7 and Table-8.

Comparatively, obtained standard deviation values are much better with McAllister's four-body model and Jouyban-Acree relations and are having a good agreement with the experimental data with the three adjustable interaction parameters. These parameters are very much useful for the chemical and industrial process and design of equipment. With this study, an increase in adjustable parameters reduces the standard deviation and enhances the correlating ability for the binary liquid mixtures.

Table-7: Calculated Values of Interaction parameters of McAllister three body and Four Body Equations for the Binary Mixtures of Propiophenone with Aniline, N-Methylaniline, N, N-Dimethylaniline and N, N-Diethylaniline.

Binary Mixture	T/K	McAllister Three Body			McAllister Four Body			
		a	b	σ	A	B	C	σ
PPH+ANILINE	303.15	2.1503	2.6499	0.0019	1.9815	2.3434	2.8042	0.0002
	308.15	1.962	2.3726	0.0023	1.8386	2.1237	2.5022	0.0002
	313.15	1.7823	2.0974	0.0025	1.699	1.8978	2.205	0.0002
	318.15	1.6107	1.8267	0.0024	1.5627	1.6775	1.9094	0.0001
PPH+N-MEA	303.15	1.6273	1.7869	0.0009	1.6065	1.6877	1.8381	0.0001
	308.15	1.5547	1.6631	0.0018	1.5387	1.5836	1.7161	0.0001
	313.15	1.4671	1.5527	0.0018	1.471	1.4803	1.5938	0.0002
	318.15	1.3867	1.4353	0.0022	1.4021	1.3775	1.47	0.0001
PPH+NN-DMA	303.15	1.3589	1.2442	0.0005	1.4007	1.2928	1.2297	0.0001
	308.15	1.3017	1.1721	0.0012	1.3514	1.2192	1.1559	0.0001
	313.15	1.2432	1.0975	0.0017	1.2989	1.1471	1.0777	0.0001
	318.15	1.1848	1.0254	0.0023	1.2471	1.0756	1.0016	0.0002
PPH+NN-DEA	303.15	1.5209	1.6135	0.0054	1.498	1.574	1.6146	0.0002
	308.15	1.4422	1.4986	0.0034	1.4397	1.4674	1.504	0.0001
	313.15	1.3643	1.3849	0.0014	1.3815	1.3624	1.3937	0.0002
	318.15	1.2906	1.2753	0.0017	1.3185	1.2641	1.2804	0.0003

Table-8: Calculated Values of Interaction Parameters of Auslander and Jouyban-Acree equations for the Binary Mixtures of Propiophenone with Aniline, N-Methylaniline, N, N-Dimethylaniline and N, N-Diethylaniline.

Binary Mixture	T/K	Auslander Equation				Jouyban-Acree Equation			
		B12	A21	B21	σ	A0	A1	A2	σ
PPH+ANILINE	303.15	1.0157	0.9482	0.9854	0.0026	66.1868	16.8143	0.7687	0.0002
	308.15	1.0175	0.9471	0.9853	0.0027	48.6729	11.5753	1.0882	0.0002
	313.15	1.022	0.9356	0.9778	0.0033	28.1379	6.6402	2.2588	0.0002
	318.15	0.0707	0.0696	12.5029	0.0031	7.5925	3.0158	5.8035	0.0001
PPH+N-MEA	303.15	0.3648	0.299	2.3848	0.0011	-13.8701	-2.7334	-2.7884	0.0001
	308.15	0.1779	0.1543	4.2745	0.0013	-17.7313	-2.4692	-4.581	0.0001
	313.15	0.102	0.101	5.5888	0.0016	-21.2056	-2.0448	-7.5051	0.0002
	318.15	0.135	0.14	2.1938	0.0016	-24.3984	-1.6514	-11.6921	0.0001
PPH+NN-DMA	303.15	0.8609	1.4279	1.0046	0.0006	-23.7882	-0.0562	-73.3776	0.0004
	308.15	4.8666	7.0244	0.1798	0.0011	-19.0828	-0.1516	-66.5628	0.0003
	313.15	1.1144	1.5136	0.8517	0.0021	-13.2524	-0.1754	-83.4016	0.0002
	318.15	1.1806	1.5136	0.8237	0.0027	-4.9297	0.0324	627.197	0.0004
PPH+NN-DEA	303.15	6.0009	3.2874	-0.1735	0.0005	-29.2444	-10.0341	1.0303	0.0002
	308.15	4.2828	1.7901	-0.8049	0.0002	-30.3602	-9.5487	0.2949	0.0001
	313.15	-8.0608	1.9897	4.8771	0.0003	-30.2132	-9.1968	-0.6052	0.0002
	318.15	3.5332	13.5872	0.1175	0.0011	-29.9469	-8.9747	-1.2021	0.0003

The values of deviations in viscosity ($\Delta\eta$) and excess Gibbs Energy (G^*E) concerning the mole fraction at temperatures from 303.15K to 318.15 K were fitted to the Redlich-Kister Equation²⁷ of the type are tabulated in Table-9.

Table -9: Coefficients of Redlich-Kister Polynomial Equation and Standard Deviation of Binary Systems.

Property	Temp (K)	A0	A1	A2	A3	A4	σ	A0	A1	A2	A3	A4	σ
		PPH+ANILINE						PPH+N-METHYL ANILINE					
$\Delta\eta$ (mPa.s)	303.15	-0.1238	0.0137	0.0654	-0.0096	0.0033	0.0001	-0.1365	-0.0074	0.0460	0.0084	-0.0037	0.0000
	308.15	-0.1043	0.0117	0.0699	-0.0016	-0.0006	0.0001	-0.1286	-0.0056	0.0548	0.0046	0.0094	0.0001
	313.15	-0.1023	0.0148	0.0978	-0.0108	-0.0255	0.0002	-0.1211	-0.0063	0.0747	0.0085	-0.0004	0.0001

Property	Temp (K)	A0	A1	A2	A3	A4	σ	A0	A1	A2	A3	A4	σ
	318.15	-0.0990	0.0151	0.0978	-0.0120	-0.0119	0.0001	-0.1149	-0.0053	0.0838	0.0046	0.0042	0.0001
G ^{*E} (J/mol)	303.15	7.0901	1.0985	1.0537	0.2667	0.1203	0.0009	-0.7584	-0.2921	0.6914	0.1932	-0.0328	0.0006
	308.15	5.5759	0.6412	1.0269	0.3030	0.0694	0.0009	-1.0615	-0.2614	0.8621	0.1753	0.1423	0.0016
	313.15	3.8616	0.2794	1.3568	0.1672	-0.2768	0.0018	-1.3336	-0.2521	1.2408	0.2468	-0.0224	0.0010
	318.15	2.2112	0.0123	1.4521	0.0998	-0.1562	0.0016	-1.5690	-0.2009	1.4756	0.1769	0.0376	0.0018
PPH+NN-DIETHYLANILINE							PPH+NN-DIMETHYLANILINE						
$\Delta\eta$ (mPa.s)	303.15	-0.1637	-0.0375	-0.0607	-0.0140	0.0160	0.0001	-0.1474	-0.0102	0.0164	0.0058	0.0042	0.0001
	308.15	-0.1490	-0.0408	-0.0232	-0.0028	0.0172	0.0001	-0.1374	-0.0107	0.0329	0.0044	0.0160	0.0000
	313.15	-0.1345	-0.0432	0.0142	0.0045	0.0162	0.0002	-0.1317	-0.0110	0.0509	0.0051	0.0071	0.0001
	318.15	-0.1263	-0.0436	0.0157	0.0062	0.0477	0.0002	-0.1251	-0.0121	0.0628	0.0046	0.0114	0.0001
G ^{*E} (J/mol)	303.15	-2.0682	-0.7376	-0.9036	-0.2330	0.2601	0.0015	-2.0636	0.1271	0.4005	0.0556	0.0939	0.0020
	308.15	-2.1178	-0.7576	-0.3429	-0.0269	0.2994	0.0017	-1.6601	0.1236	0.7365	-0.0541	0.2863	0.0012
	313.15	-2.0691	-0.7584	0.3070	0.0936	0.2748	0.0032	-1.1975	0.0997	1.0999	-0.1101	0.1270	0.0023
	318.15	-1.9984	-0.7323	0.4176	0.0925	0.7941	0.0046	-0.5470	0.0206	1.3803	-0.2472	0.2620	0.0013

CONCLUSION

Densities and viscosities values were measured for the studied binary liquid mixtures at temperatures, $T = (303.15 \text{ to } 318.15) \text{ K}$. The G^*E , W_{vis}/RT , H_{12} , and d_{12} values were positive for Propiopheneone + Aniline mixtures over the experimental temperature range, while they were negative for Propiophenone+N-Methylaniline, Propiophenone+N, N-Dimethylaniline and Propiophenone+N, N-Diethylaniline. The positive G^*E , W_{vis}/RT , H_{12} , and d_{12} values were attributed to the formation of the new complex, whereas negative values were due to the consequence of dominating effect. The calculated values of $\Delta\eta$ and G^*E were correlated with the Redlich-Kister polynomial equation to compute the coefficients and standard deviations. Viscosity data compared with several viscosity relations like Kendall-Monroe, Bingham, Arrhenius, Kendall and calculated the two / three adjustable interaction parameters and respective standard deviations by correlating with the McAllister three/four body models, Jouban-Acree and Auslander equations. The obtained results are useful in various industrial and chemical processes.

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